

LOW-COST CO₂ CAPTURE BY CHEMICAL LOOPING COMBUSTION OF WASTE-DERIVED FUELS

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Demonstration plant concept



November 2024

Outline

- Introduction
- Reactor system
- Fluegas cleaning system
- CO₂ processing system
- Plant layout
- Conclusion

Introduction

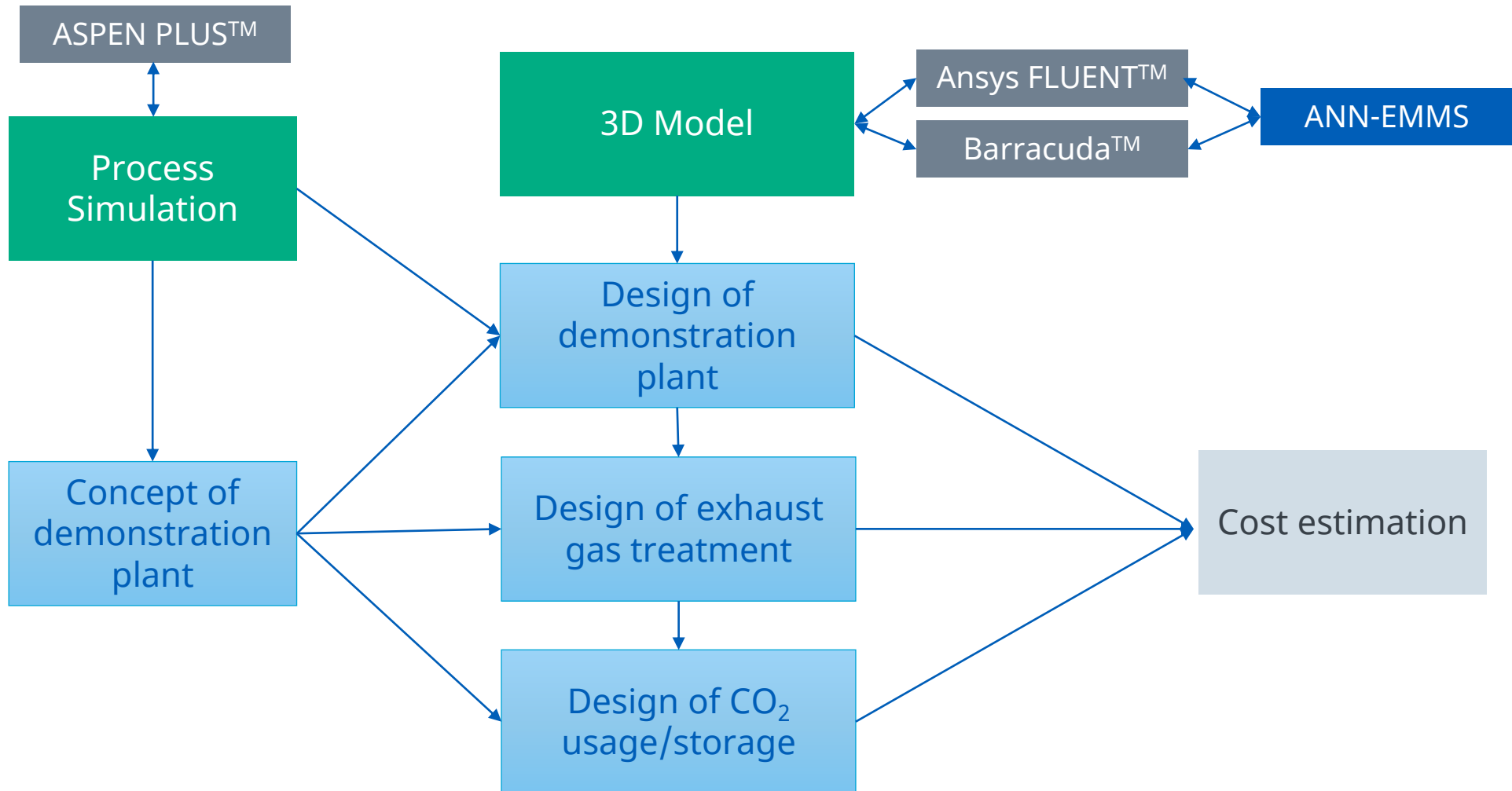
Target: 10 MW_{th} demonstration plant (TRL 7)

Fuel: Solid recovered fuel (SRF)

Work contents:

- Design of
 - Fluidized bed reactors
 - Exhaust gas treatment
 - Heat recovery
 - Usage or storage of CO₂

Basic design of a demonstration plant

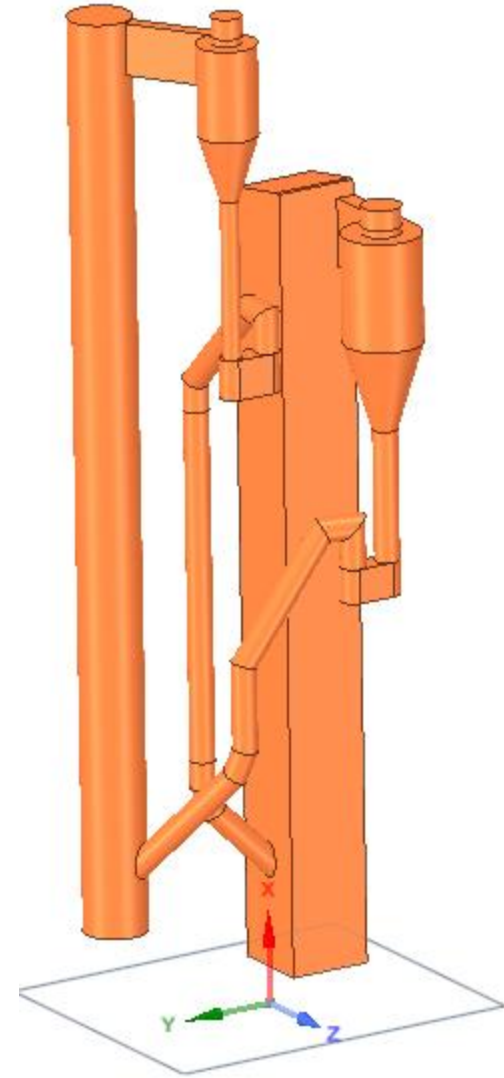


Status of concept

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Reactor system:

- Two interconnected Circulating Fluidized Bed Reactors
- Air reactor is cooled (by means of evaporator membrane walls) and rectangular in design
- Fuel reactor is round and adiabatic design
- Two cyclones separate the solids from the exhaust gas flow and transports the particles to the other reactor
- A loop seal is fitted under both cyclones to pass the particles on without nitrogen entering the fuel reactor and without CO₂ or pyrolysis gases entering the air reactor.



Heat recovery system

- Water-Steam system: 60 bar, 430 ° C (corresponding to waste-to-energy plants)
- Natural circulation boiler
- Boiler efficiency 99.7%
- Electric efficiency 30.3%
- Air reactor:
 - External economizer 1
 - Superheater 1.3, 2
 - Evaporator:
 - Air reactor membrane walls
 - 1th pass membrane walls
 - 2nd pass membrane walls
- Fuel reactor:
 - External economizer 2, 3, 4
 - Superheater 1.1, 1.2
 - Evaporator:
 - 1st pass membrane walls with middle wall
 - 2nd pass membrane walls

Post oxidation chamber

- Unconverted pyrolysis gases (H_2 , CO , CH_4 and other hydrocarbons) are oxidised in a combustion chamber using pure oxygen to H_2O and CO_2 .
- The post oxidation chamber (POC) leads to a complete fuel conversion and increases the energy conversion
- Exhaust gas is recirculated to control the combustion temperatures. The design of the POC is based on a gas combustion chamber

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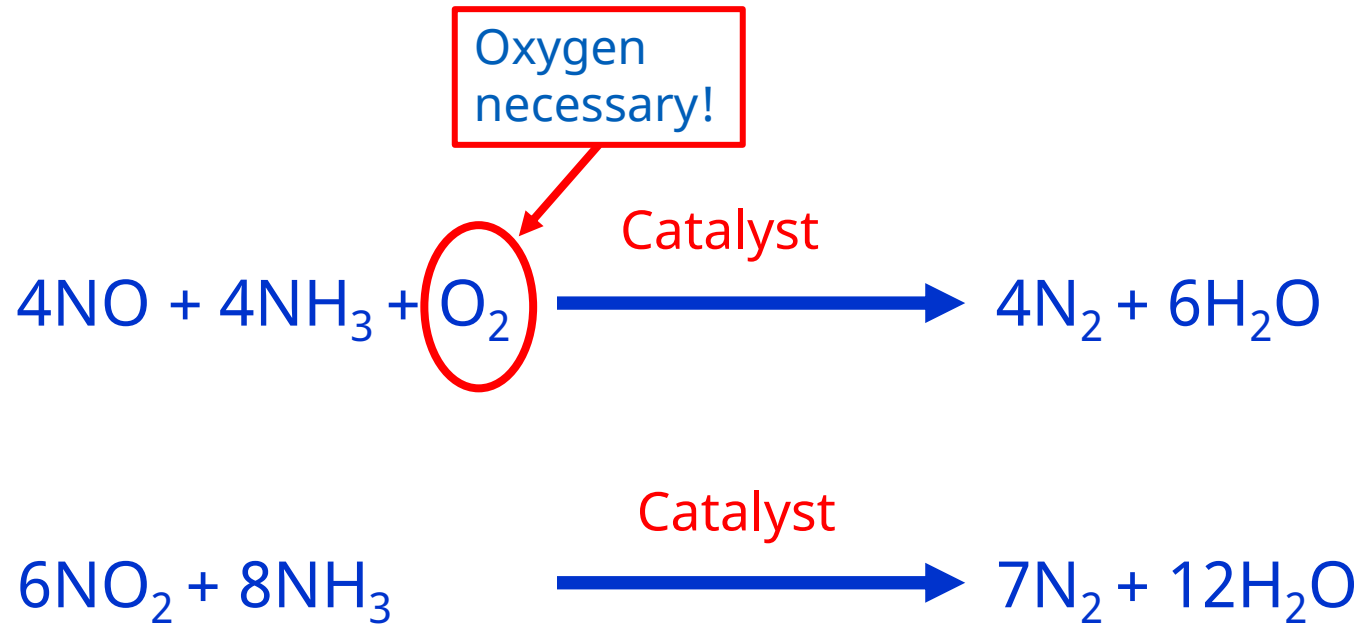
Status of flue gas cleaning system

- Cleaning of FR flue gas (after Post oxidation chamber)
 - Removal of:
 - NO_x
 - SO_x
 - HCl , HF
 - Hg and PCDD/PCDF
 - Dust
- Cleaning of air reactor
 - Removal of:
 - Dust

Equipment & Process

- Low dust **S**elective **C**atalytic **R**eduction (SCR)
- Main components:
 - Ammonia Injection
 - Static Mixer
 - Reactor Housing
 - 1 Catalyst Layer

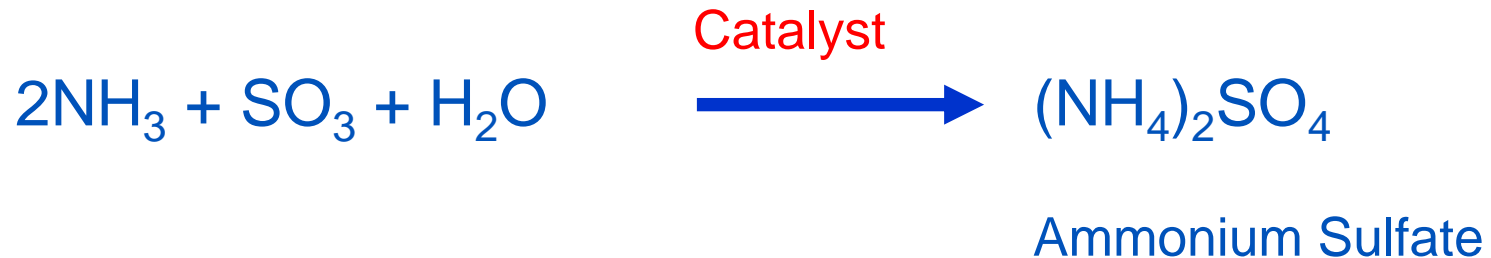
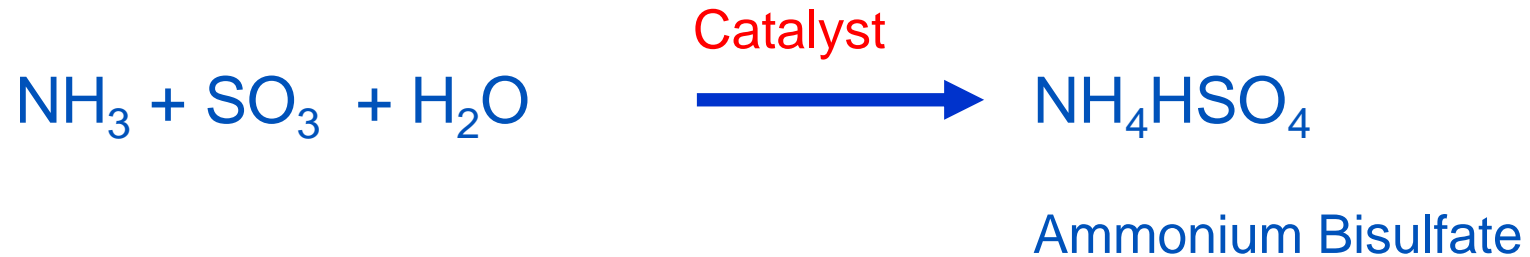
Chemical Reactions



Catalyst Operation Temperature

- Flue gas temperature range
- $> 265^{\circ} \text{ C}$ to avoid ammonium bisulfate formation
- $< 440^{\circ} \text{ C}$ to avoid catalyst material fusion

Parallel Reactions



Both salts form at flue gas temperatures below 320°C

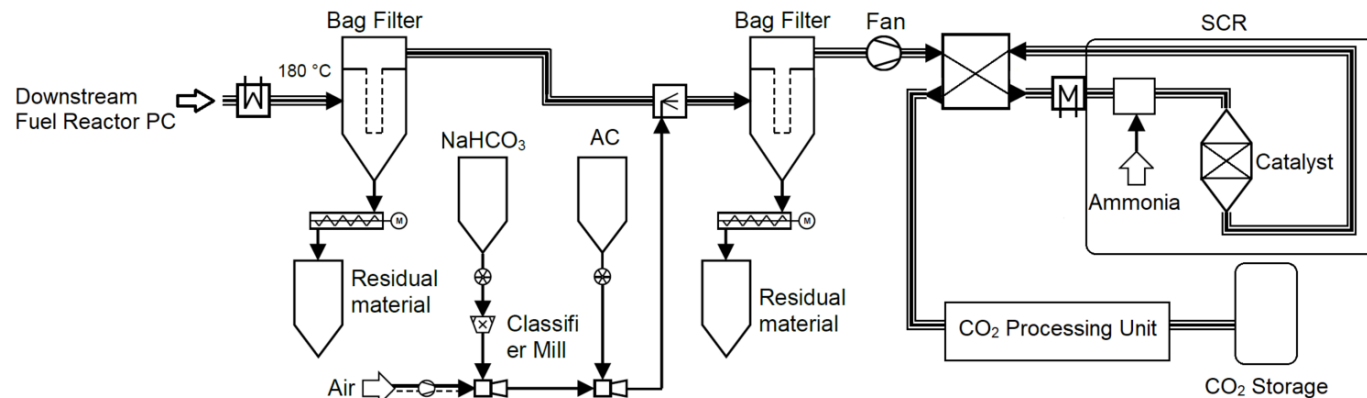
Dry sorption using sodium bicarbonate

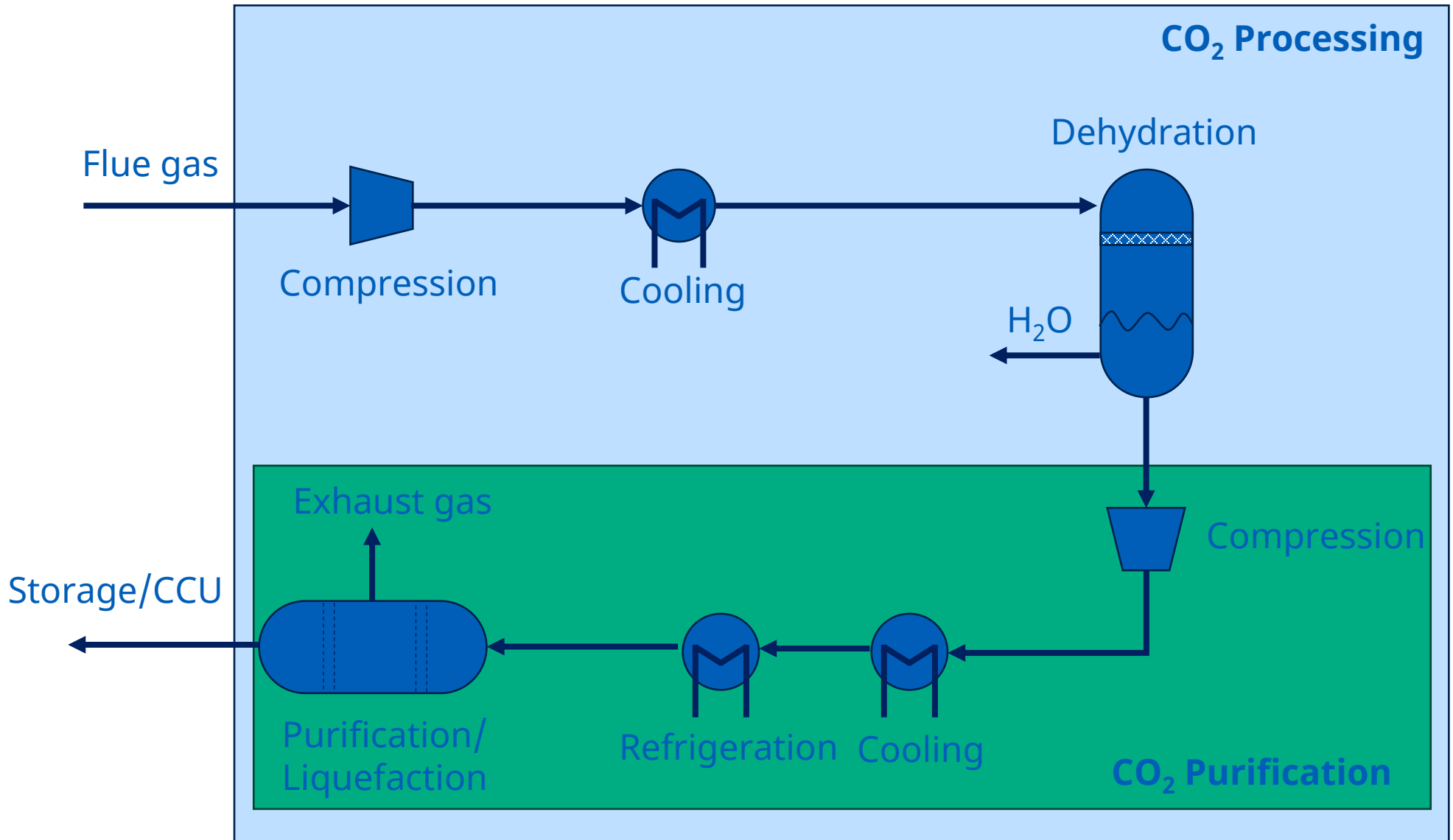
- **Dry sorption:**

- Dosing of sodium bicarbonate: separation of HCl, HF and SO_x
- Dosing of activated carbon: separation of Hg and PCDD/PCDF

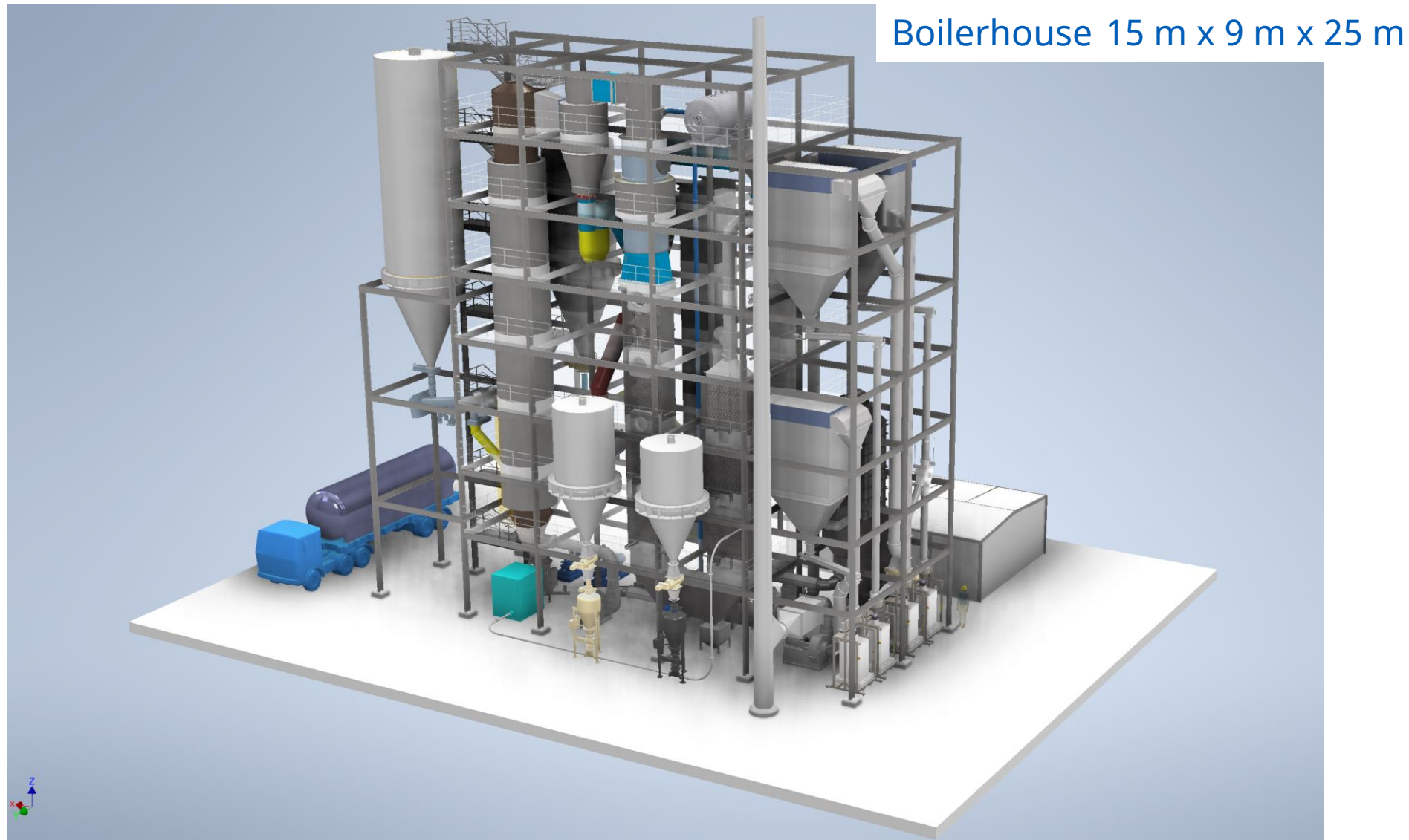
Fabric filter:

- Separation of fly ash, dust and reaction products
- Outward transfer of residues into the residues silo
- Recirculation of residues into the circulating fluidized bed reactor





Layout reactorsystem



Conclusion

- Two interconnected CFBs
- Water-Steam system corresponding to waste-to-energy plants to prevent corrosion
- Post oxidation chamber oxidise not converted pyrolysis gas
- SCR system to remove NO_x
- Sodium bicarbonate & activated carbon in two-pass reactor to remove SO_x, HCl, HF, Hg and PCDD/PCDF
- Fabric filters to remove particles

Thank you for your attention!
Do you have any questions?

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